# Hydrodeoxygenation of lignin-derived guaiacol on supported Pd and Ni catalysts using neat and phosphorus-modified $\gamma$ -alumina supports

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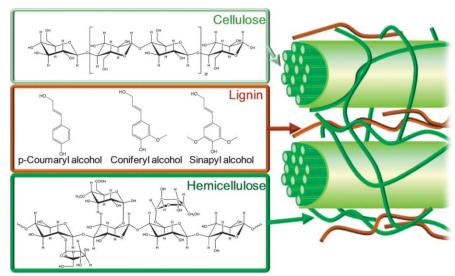


# Lignocellulose as source of carbon and energy

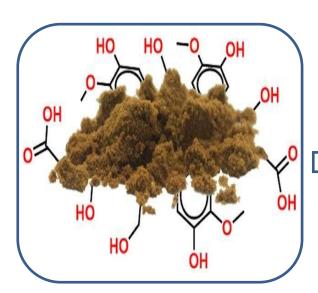
#### **Current carbon and energy resources**

# Coal 28 % Petroleum 34 % Renewable 10 % Nuclear 4 % Natural gas 24 % Wind 18 %

#### **Structure of lignocellulose**



Chem. Soc. Rev. 41 (2012) 8075



Distribution of energy sources

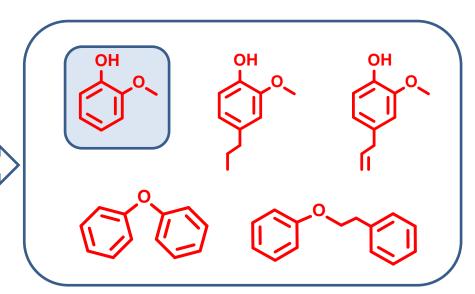
(BP Statistical Review of World Energy)

chemical/thermal

Geothermal and Biomass 9 %

Solar 7 %

depolymerization

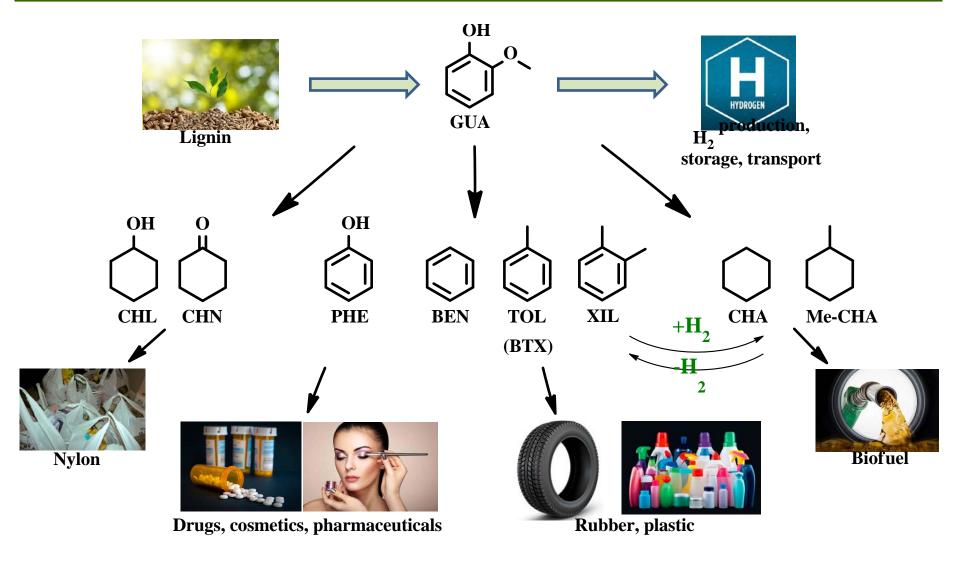


Lignin

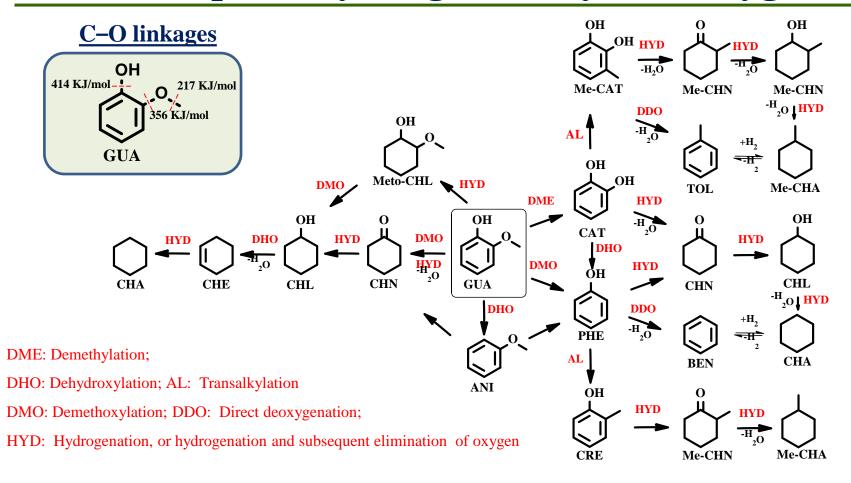
**Bio-oxygenates** 

Chem. Rev. 110 (2010) 3552; App. Cat. B 257 (2019) 117936

#### **Guaiacol-based chemicals**



#### Reaction pathways of guiacol hydrodeoxygenation



ChemCatChem 4 (2012) 64; ACS Catal. 3 (2013) 1774; App. Cat. A 512 (2016) 93; App. Cat. B 270 (2020) 118890

#### **Objectives:**

- > to convert GUA to value-added materials
- > to elucidate the pathways of product formation
- > optimization of HDO catalysts

# **Catalyst preparation**

Catalyst	Precursor	Support	
Pd/Al <sub>2</sub> O <sub>3</sub>	$Pd(NH_3)_4(NO_3)_2$		
Ni/Al <sub>2</sub> O <sub>3</sub>	$Ni(NO_3)_2) \cdot 6H_2O$	γ–Al <sub>2</sub> O <sub>3</sub> (Alfa Aesar)	
<b>Pd/Al<sub>2</sub>O<sub>3</sub> (P)</b>	$Pd(NH_3)_4(NO_3)_2$	γ-Al <sub>2</sub> O <sub>3</sub> (Alfa Aesar)	
$Ni/Al_2O_3(P)$	$Ni(NO_3)_2) \cdot 6H_2O$	impregnated with $H_3PO_4$ solution, dried and calcined (550 °C, 4h)	

➤ Impregnation: metal salt solution
 ➤ Calcination: 350 °C (Pd), 450 °C (Ni), 4h

PdO NiO
NiO

> In situ reduction: 350 °C (Pd), 450 °C (Ni), 2h,  $H_2 \longrightarrow \frac{Pd^0}{Ni^0}$ 

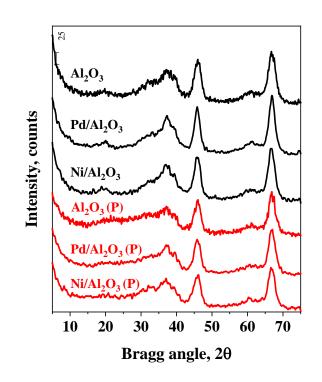
> Catalytic experiments were carried out in a continuous flow-through fixed-bed microreactor

#### Catalyst characterization

#### Metal and P content; Specific surface area (SSA)

Supports and catalysts	Metal content wt%	P content wt%	SSA m²/g
Al <sub>2</sub> O <sub>3</sub>	-	-	196
Pd/Al <sub>2</sub> O <sub>3</sub>	0.47	-	194
Ni/Al <sub>2</sub> O <sub>3</sub>	5.21	-	192
$Al_2O_3(P)$	-	-	167
Pd/Al <sub>2</sub> O <sub>3</sub> (P)	0.49	4.87	163
Ni/Al <sub>2</sub> O <sub>3</sub> (P)	5.06	4.82	165

#### X-ray diffraction (XRD)



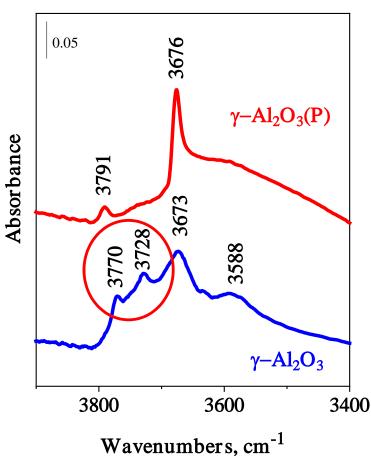
- Metal impregnation has no influence on SSA
- ➤ Impregnation of Al<sub>2</sub>O<sub>3</sub> support with H<sub>3</sub>PO<sub>4</sub> solution reduces SSA

- ightharpoonup Al<sub>2</sub>O<sub>3</sub> is the only detectable phase
- ➤ NiO and PdO crystallites are well dispersed on the Al<sub>2</sub>O<sub>3</sub> surface

#### Surface structure of phosphated γ-alumina

FT-IR spectra in the vOH region (ev. 450 °C, 1 h)

Phosphoric acid reacts with the hydroxyls of alumina monomeric and polymeric phosphate species are formed<sup>a</sup>



**OH groups** (G. Busca, Cat. Today 226 (2014) 2.)

γ-Al<sub>2</sub>O<sub>3</sub>

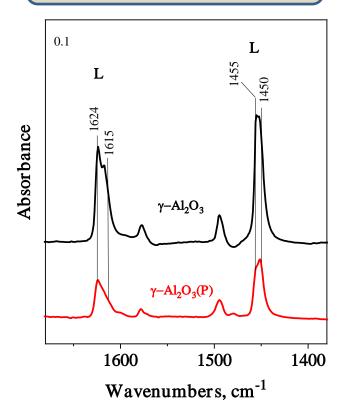
- 3770 cm<sup>-1</sup>, □-O-Al<sup>IV</sup>-OH, (terminal)<sub>tetr</sub> with vacancy
- 3728 cm<sup>-1</sup>, Al<sup>VI</sup>-OH, (terminal)<sub>oct</sub> without and with vacancy
- 3673 cm<sup>-1</sup>, Al-O(H)-Al, bridged
- 3588 cm<sup>-1</sup>, triple-bridged

 $\gamma$ -Al<sub>2</sub>O<sub>3</sub>(P)

- 3791 cm<sup>-1</sup>, Al<sup>IV</sup>-OH, (terminal)<sub>tetr</sub>
- 3676 cm<sup>-1</sup>, P-OH on phosphates

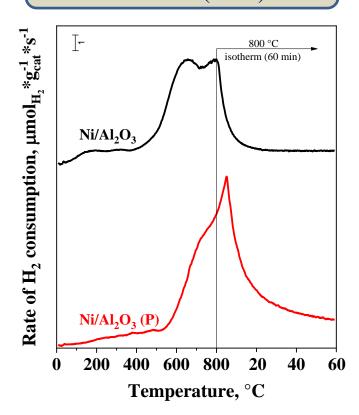
## Catalysts acidity and reducibility

# FT-IR spectra of adsorbed pyridine



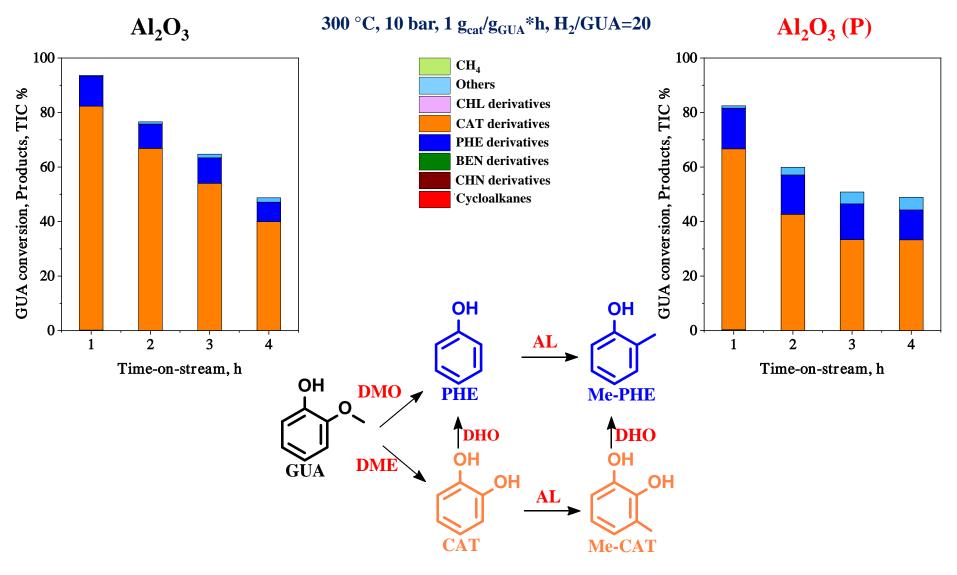
- ➤ On the Al<sub>2</sub>O<sub>3</sub> (P) support the intensity of bands at 1450, 1455 cm<sup>-1</sup> and 1615, 1624 cm<sup>-1</sup> is lower lower Lewis acidity
- ➤ Phosphorus modification reduces the Lewis acidity of the alumina support

# **Temperature-programmed** reduction (TPR)



- Pd can be reduced at room temperature (not shown in the figure)
- ➤ The degree of reduction at 450 °C:
  - $Ni/Al_2O_3 \sim 4.5 \%$  of Ni (H/Ni=0.09)
  - $Ni/Al_2O_3(P) \sim 0.5\% (H/Ni=0.01)$

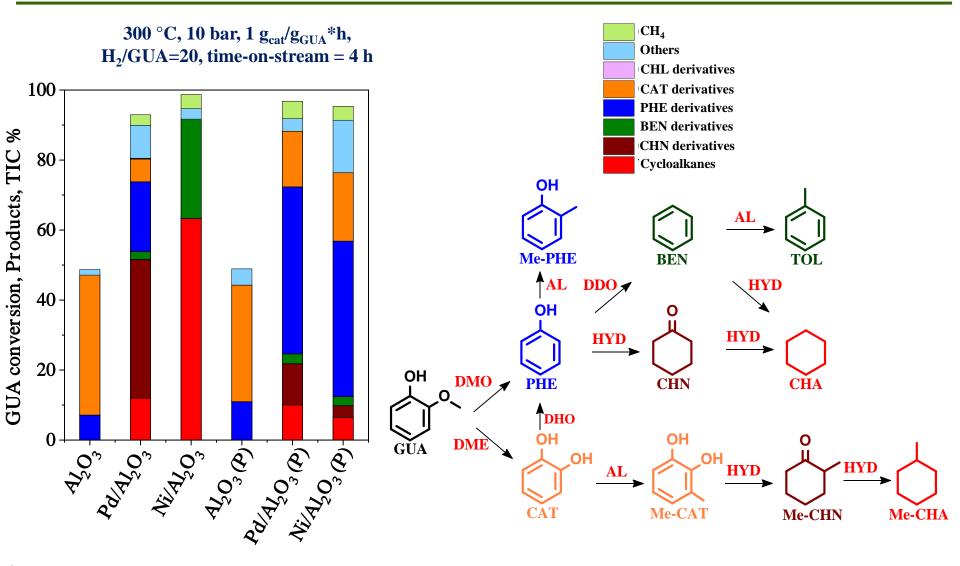
## Activity of Al<sub>2</sub>O<sub>3</sub> and Al<sub>2</sub>O<sub>3</sub> (P) supports



- ➤ Demethylation (DME) and transalkylation (AL) are the main reactions
- > CAT derivatives are the main products

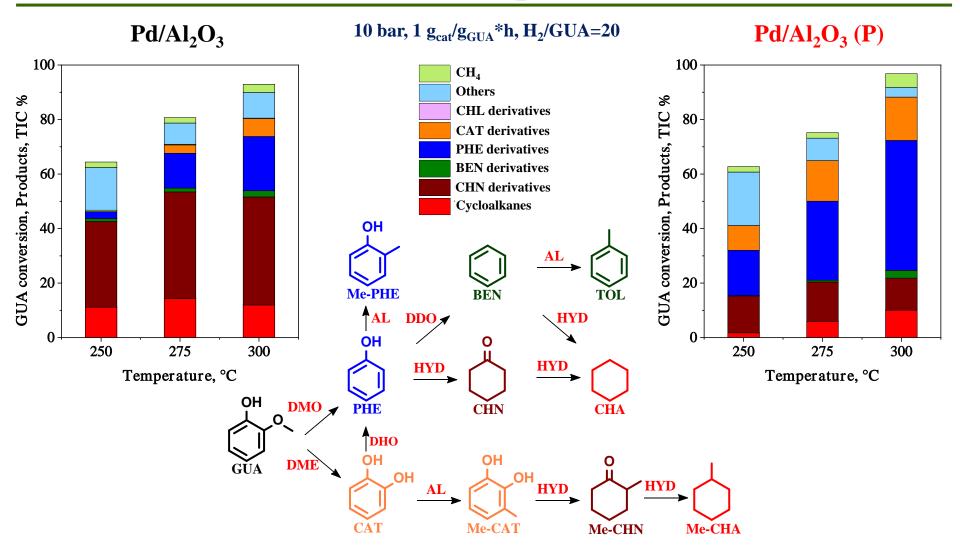
- Demethoxylation (DMO) and dehydroxylation (DHO) also takes place
- > PHE derivatives were also formed

#### **Comparison of catalysts activity**



- ➤ Cyclohexanones and cycloalkanes are the main products on Pd/Al<sub>2</sub>O<sub>3</sub>
- O-free compounds were mainly formed on Ni/Al<sub>2</sub>O<sub>3</sub>
- ➤ Aromatics (phenols, catechols) were formed on Pd/Al<sub>2</sub>O<sub>3</sub> (P) and Ni/Al<sub>2</sub>O<sub>3</sub> (P)

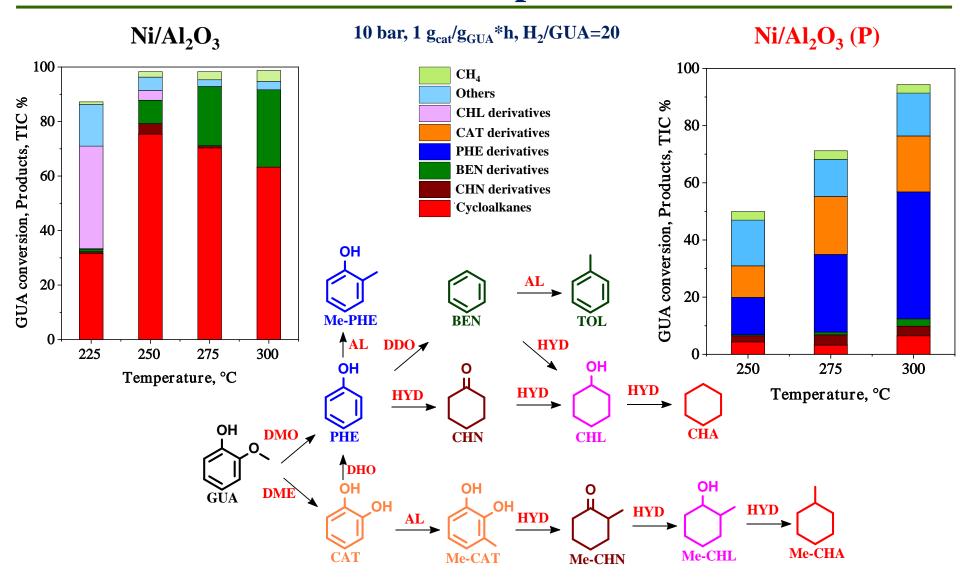
#### **Effect of temperature**



- The yield of CHN derivatives is high at 250 °C and does not change with temperature
- ➤ 1-Methoxycyclohexane and 2-methoxycyclohexanone were also formed (not shown)

- The yield of aromatics (phenols, catechols) increases with temperature
- ➤ 1,2-Dimethoxybenzene was also formed at lower temperature (not shown)

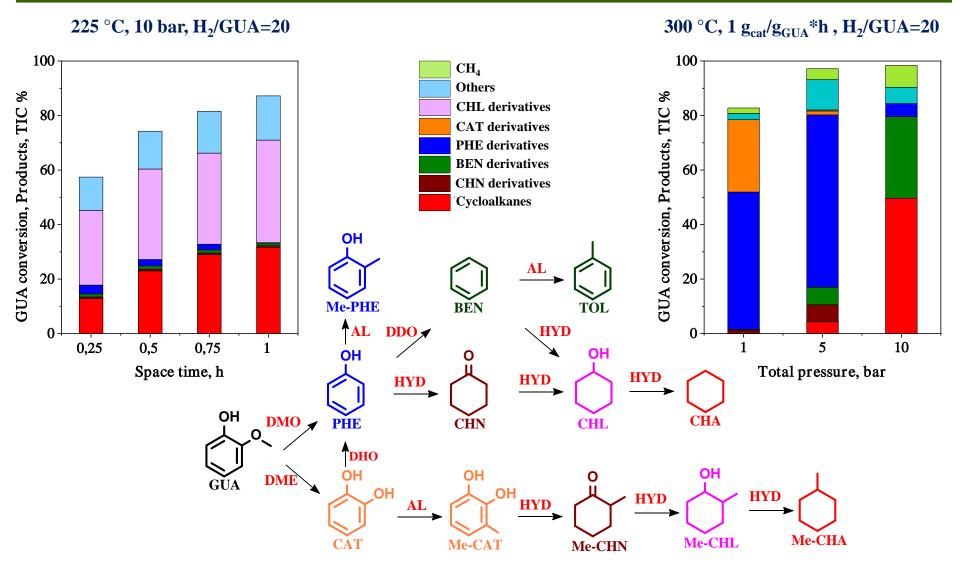
#### **Effect of temperature**



- ➤ At 225 °C cyclohexanols were the main products
- ➤ At 250 °C high yield and selectivity to CHA
- ➤ With temperature the yield of benzenes increased as dehydrogenation is accelerated

➤ The yield of aromatics (phenols, catechols) increases with temperature

# Effect of space time and total pressure on Ni/Al<sub>2</sub>O<sub>3</sub>



- At lower space time phenol intermediates appear in the product mixture
- ➤ GUA hydrodeoxygenation to CHL and CHA proceeds through PHE intermediates

- ➤ At lower pressure the hydrogenation activity is lower
- With total pressure more hydrogenated products were formed

#### **Conclusions**

- ✓ The sequential steps of GUA hydrodeoxygenation can be controlled by using noble and non-noble metal and modifying the alumina support.
- ✓ Both neat and phosphorus-modified Al<sub>2</sub>O<sub>3</sub> supports are active in demethylation of GUA to form catechol.
- ✓ Pd/Al<sub>2</sub>O<sub>3</sub> catalyst shows high activity and selectivity in GUA hydrodeoxygenation to cyclohexanones.
- ✓ Ni/Al<sub>2</sub>O<sub>3</sub> catalyzed hydrodeoxygenation of GUA to O-free compounds like cyclohexane.
- ✓ Pd and Ni supported on phosphorus-modified alumina behave similarly, they are selective to aromatics.
- ✓ Pd/Al<sub>2</sub>O<sub>3</sub>(P) and Ni/Al<sub>2</sub>O<sub>3</sub>(P) catalysts remain active in demethylation and demethoxylation, but lose their ability to hydrogenate the aromatic ring. (low hydrogenation activity, and/or weaker interaction between substrate molecules and phosphated support)



#### Thank you for your kind attention!



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