

Hydroconversion of lignin-derivative guaiacol over alumina-supported Pd and Ni catalysts



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Introduction



- Liquid hydrocarbons obtained by total HDO of GUA can be used as biofuel. The selective partial HDO of GUA results in the formation of oxygenated products like cyclohexanone (CHN) and cyclohexanol (CHL). These oxygenates are precursors of adipic acid, caprolactane and industrial precursors of nylons. The demethylation and/or demethoxylation of GUA leads to the formation of aromatic products like benzene, toluene, xylenes (BTX), phenols and catechols, which are important precursors for many commercial chemicals, pharmaceuticals and polymers [2,3,4].
- In the present study γ -Al₂O₃ and phosphorous-modified γ -Al₂O₃-supported Pd and Ni catalysts were investigated in HDO of GUA using a fixed-bed flow-through microreactor. [1] M.J. Climent et al. Green Chem. 2014, 16, 516; [2] H. Zhou et al. Appl. Catal. B 2020, 270, 118890; [3] H. Wang et al. ChemSusChem 2017, 10, 1846; [4] G.Y. Xu et al. Green Chem. 2016, 18, 5510

Catalysts preparation and characterization						
X-ray diffraction (XRD)	Temperature-programmed	Metal and P content; Specific	FT-IR spectra of adsorbed	FT-IR spectra in the		
	reduction (H ₂ -TPR)	surface area (SSA)	pyridine	vOH region		
0	7 . 800 °C	Supports Metal P SSA				



- $\succ \gamma$ -Al₂O₃ is the only detectable phase of catalysts with low metal loading (NiO and PdO crystallites are well dispersed). > The XRD pattern of $20Ni/Al_2O_3$
- and $20Ni/Al_2O_3(P)$ catalysts show the reflections of NiO (NiO particle size was about 30 nm).



 \succ The catalysts were in situ reduced at 450 °C in the reactor before catalytic run. \succ The degree of reduction at 450 °C: 5Ni/Al₂O₃ ~ 4.5 % of Ni (H/Ni=0.09) $5Ni/Al_2O_3(P) \sim 0.5\%$ (H/Ni=0.01) $5Ni/Al_2O_3(P)$ (550) ~ 3.5% (H/Ni=0.07) > Metal impregnation has no influence on SSA and 20Ni/Al₂O₃ ~ 68 % (1.37 H/Ni) $20Ni/Al_2O_3(P) \sim 65\% (1.3 H/Ni)$

and catalysts	content wt%	content wt%	m²/g
Al_2O_3	-	-	196
Pd/Al ₂ O ₃	0.47	-	194
5Ni/Al ₂ O ₃	5.21	-	192
20Ni/Al ₂ O ₃	~20	-	190
$Al_2O_3(P)$	-	4.85	167
$Pd/Al_2O_3(P)$	0.49	4.87	163
5Ni/Al ₂ O ₃ (P)	5.06	4.82	165
20Ni/Al ₂ O ₃ (P)	~20	4.82	131

- \succ Commercial γ -Al₂O₃ and phosphorous (P)modified γ -Al₂O₃ were used as support.
- > The phosphorous (P) modification was done with H_3PO_4 solution.
- > The SSA decreased upon P-modification.
- > The Pd- and Ni-containing catalysts were prepared by wet impregnation method.
- pore volume.
- > Catalytic experiments were carried out in a continuous flow-through fixed-bed microreactor.



> On Al₂O₃ (P) support the intensity of bands at 1450, 1455 cm⁻¹ and 1615, 1624 cm⁻¹ is lower, indicating its lower Lewis acidity. > Phosphorus modification reduces the Lewis acidity of the alumina support.



the hydroxyls of alumina and monomeric and polymeric phosphate species are formed.



- Over Pd/Al₂O₃ catalyst CHN derivatives were the main products at 300 °C. At higher temperatures (325 and 350 °C) the yield of PHE derivatives increased.
- > O-free compounds like cyclohexane (CHA) and Me-CHA

Reaction conditions: 300 °C, 10 bar, 1 g_{cat}/g_{GUA}*h, H₂/GUA: 20

- > Demethylation (DME) and transalkylation (AL) are the main reactions over Al_2O_3 and Al_2O_3 (P) supports.
- \succ CHN and cycloalkanes are the main products on Pd/Al₂O₃
- \triangleright O-free compounds were mainly formed on Ni/Al₂O₃.
- Aromatics (phenols, catechols) were formed on P modified catalysts.

> $5Ni/Al_2O_3$ and $20Ni/Al_2O_3$ catalysts were stable; their activity did not change significantly with TOS.

225 °C, 10 bar, H₂/GUA=20

300 °C, 1 g_{cat}/g_{GUA} *h , H₂/GUA=20

- > At lower space time phenol and benzene intermediates appear in the product mixture. GUA hydrodeoxygenation to CHL and CHA proceeds through PHE and BEN intermediates.
- \succ At lower pressure the hydrogenation activity is lower. At 5 bar total pressure phenols, at atmospheric pressure phenols and catechols were the main products.
- \succ With total pressure more hydrogenated products were formed.

were mainly formed over 5Ni/Al₂O₃ and 20Ni/Al₂O₃ at 250 – 300 °C. With temperature the yield of benzenes increased as dehydrogenation of cyclohexanes is accelerated. At 225 °C cyclohexanols were the main products.

> Aromatics (phenols, catechols) were formed on P modified catalysts. The amount of PHE derivatives increased with temperature.

DME: Demethylation; **DMO:** Demethoxylation DDO: Direct deoxygenation; Alkylation AL: HYD: Hydrogenation, or hydrogenation and subsequent elimination of oxygen

Conclusions

- The sequential steps of GUA hydroconversion can be controlled by using noble and nonnoble metal and modifying the alumina support.
- \blacktriangleright Demethylation of GUA on Al₂O₃ and phosphorous modified Al₂O₃(P) supports leads to catechol formation.
- \blacktriangleright Pd/Al₂O₃ catalyst shows high activity and selectivity in GUA HDO to cyclohexanones.
- \blacktriangleright Ni/Al₂O₃ catalyzed hydroconversion of GUA to O-free compounds like cyclohexane.
- \blacktriangleright At lower temperature and space time cyclohexanols were formed in large amounts.
- > Pd and Ni supported on phosphorus-modified alumina behave similarly, they are selective to aromatics.
- \geq Pd/Al₂O₃(P) and Ni/Al₂O₃(P) catalysts remain active in demethylation and demethoxylation, but lose their ability to hydrogenate the aromatic ring. (low hydrogenation activity, and/or weaker interaction between substrate molecules and phosphated support)

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